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SCR Catalyst Management and Improvement to Achieve and Maintain Mercury Oxidation Levels



Christopher Bertole

Cormetech, Inc.

Workshop "Flue Gas Cleaning 2013"

- **Background**
 - MATS
 - SCR Hg Oxidation Co-Benefit
 - Key Differences Between Hg and NO_x Control
- **Catalyst Management for NO_x, Hg, SO₃ Control**
 - Assess Unit Requirements
 - Characterize Installed Catalyst
 - Select Optimal Catalyst Action
- **Summary**

Presentation Outline



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MATS

Mercury and Air Toxics Standard

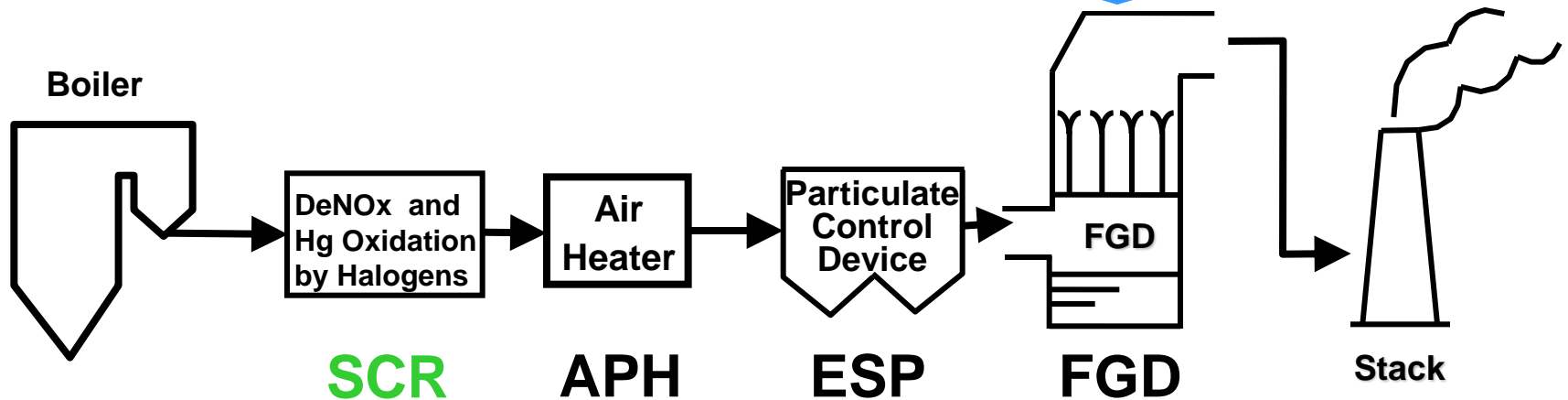
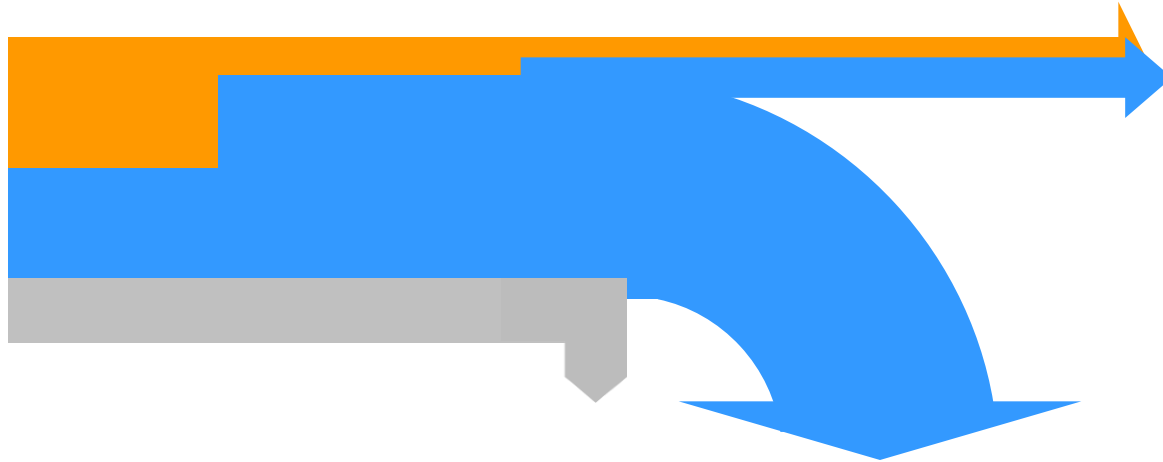


- **Focuses on:**
 - Hg
 - HCl (as a surrogate for acid gas HAP)
 - Filterable PM (as a surrogate for non-Hg HAP metals)
- **Requires compliance by 2015**
 - Published in US Federal Register on February 16, 2012
 - Provides utilities with 3-year period to achieve compliance
 - 1 additional year is available (i.e., comply by 2016), if needed for technology installation
- **Limits stack Hg emissions for existing units to:**
 - 1.2 lbs Hg/Tbtu
 - 30 operating day rolling average basis

SCR Co-Benefit for Hg Removal



- ① Elemental
- ② Oxidized
- ③ Particle bound



Key Differences for Hg vs. NOx

Hg Control Requires a Full System View

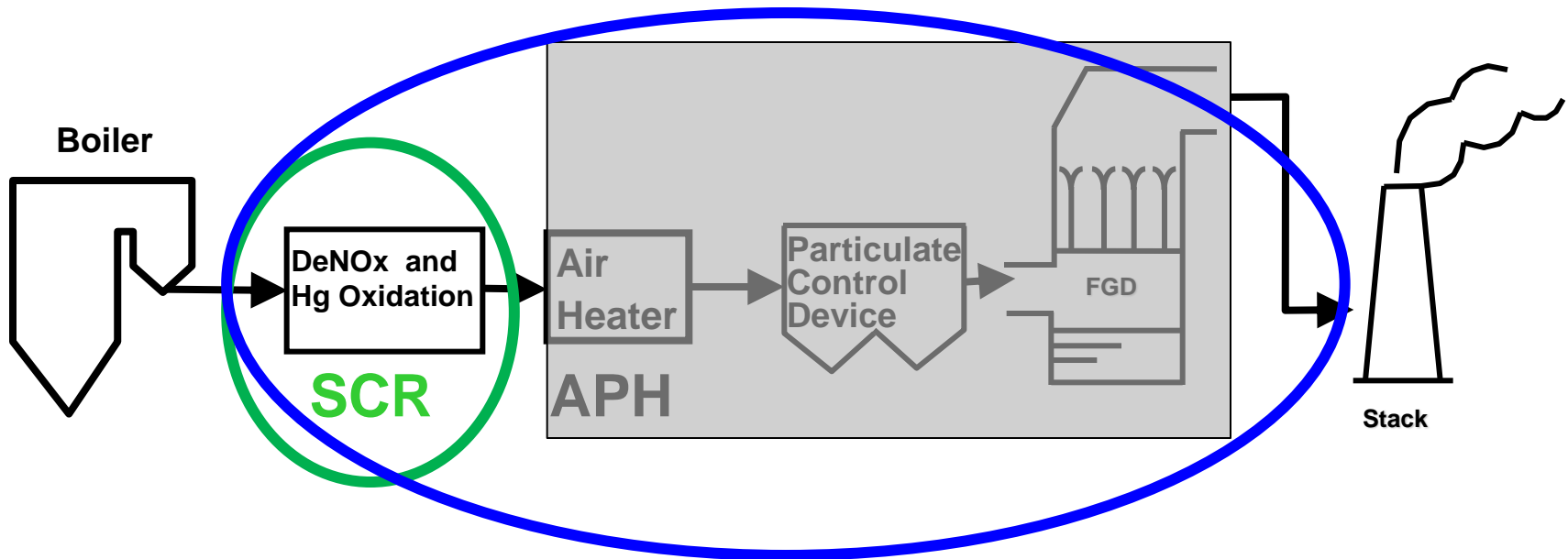


- **DeNOx**

- Performance requirements for the SCR are typically well defined due to sole role of the SCR for NOx reduction

- **Hg**

- Performance requirements for the SCR typically not as well defined due to roles of downstream equipment in total compliance



Key Differences for Hg vs. NOx

More Factors Influence Hg Oxidation



DeNOx

– Key Parameters

- NOx inlet
 - Efficiency
 - Slip
- } *Performance Threshold*
- Temperature
 - SO₂ conversion (formulation)
 - Fuel → contaminants → K/Ko
 - Reactor condition
 - O₂, H₂O, SO₂ (lower impact)

Hg

– Key Parameters

- NOx inlet
 - Efficiency
 - Slip
- } *NH₃*
- Hg oxidation → Performance Threshold
 - Temperature
 - SO₂ conversion (formulation)
 - Fuel → contaminants → K/Ko
 - Reactor condition
 - Halogen (Fuel or additive)
 - Layer position (NH₃)
 - CO
 - O₂, H₂O, SO₂ (can be larger impact)

Key Differences for Hg vs. NOx

Hg Ox Catalyst Potential, K/AV



- **Hg Oxidation K_{HgOx}/AV defines:**
 - Capacity for X% Hg oxidation
- **Activity, K_{HgOx} , depends on:**
 - Catalyst composition and age
 - Flue gas conditions (+HCl, HBr, NH₃, CO, SO₂, HC)
- $AV = \text{Area Velocity} = (\text{Gas Flow}) / (\text{Total GSA})$
- First order rate equation can be applied for Hg oxidation tests, *but be careful! This K value is strongly condition dependent!*

$$\frac{K_{HgOx}}{AV} = -\ln[1 - \% HgOx]$$

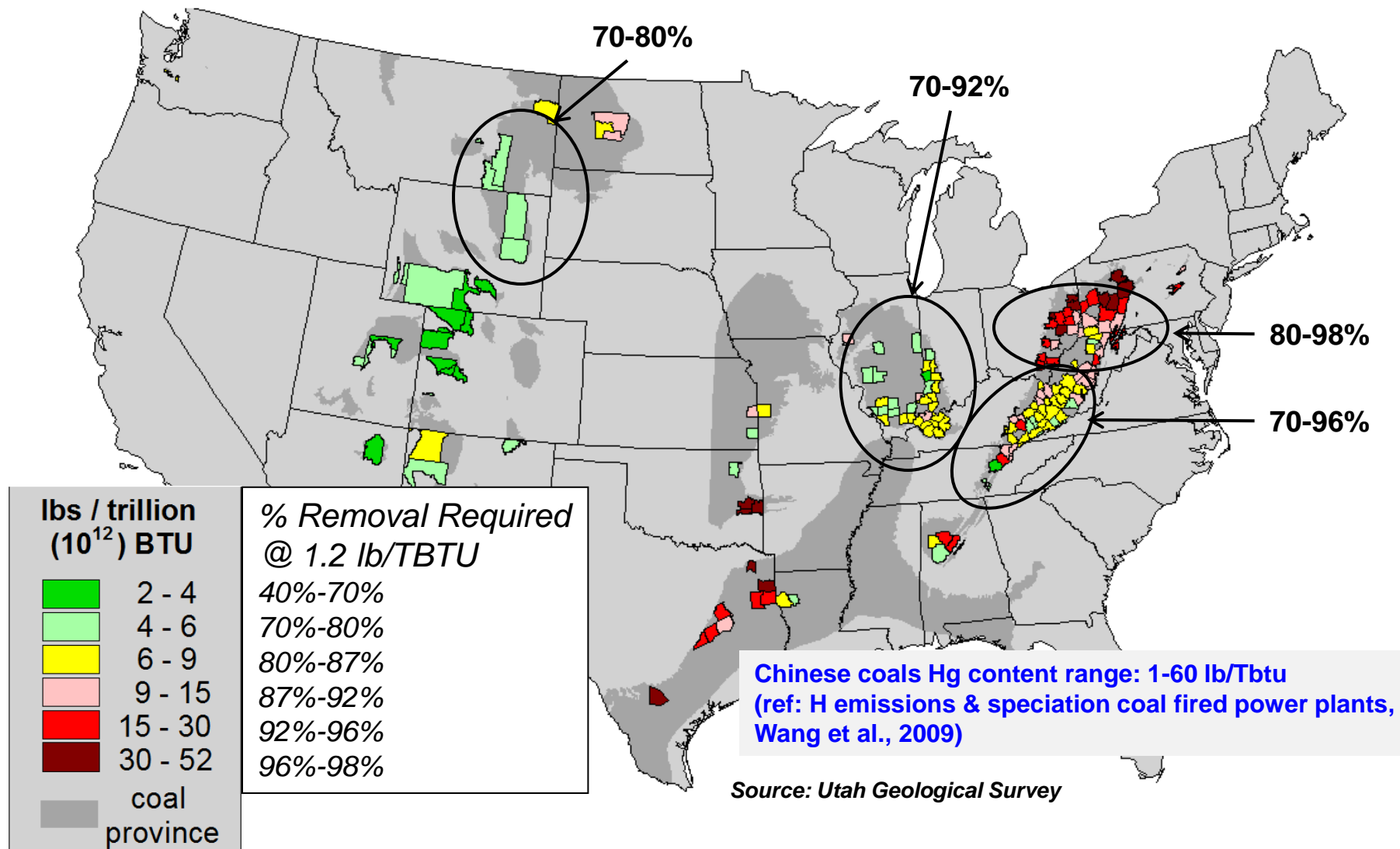
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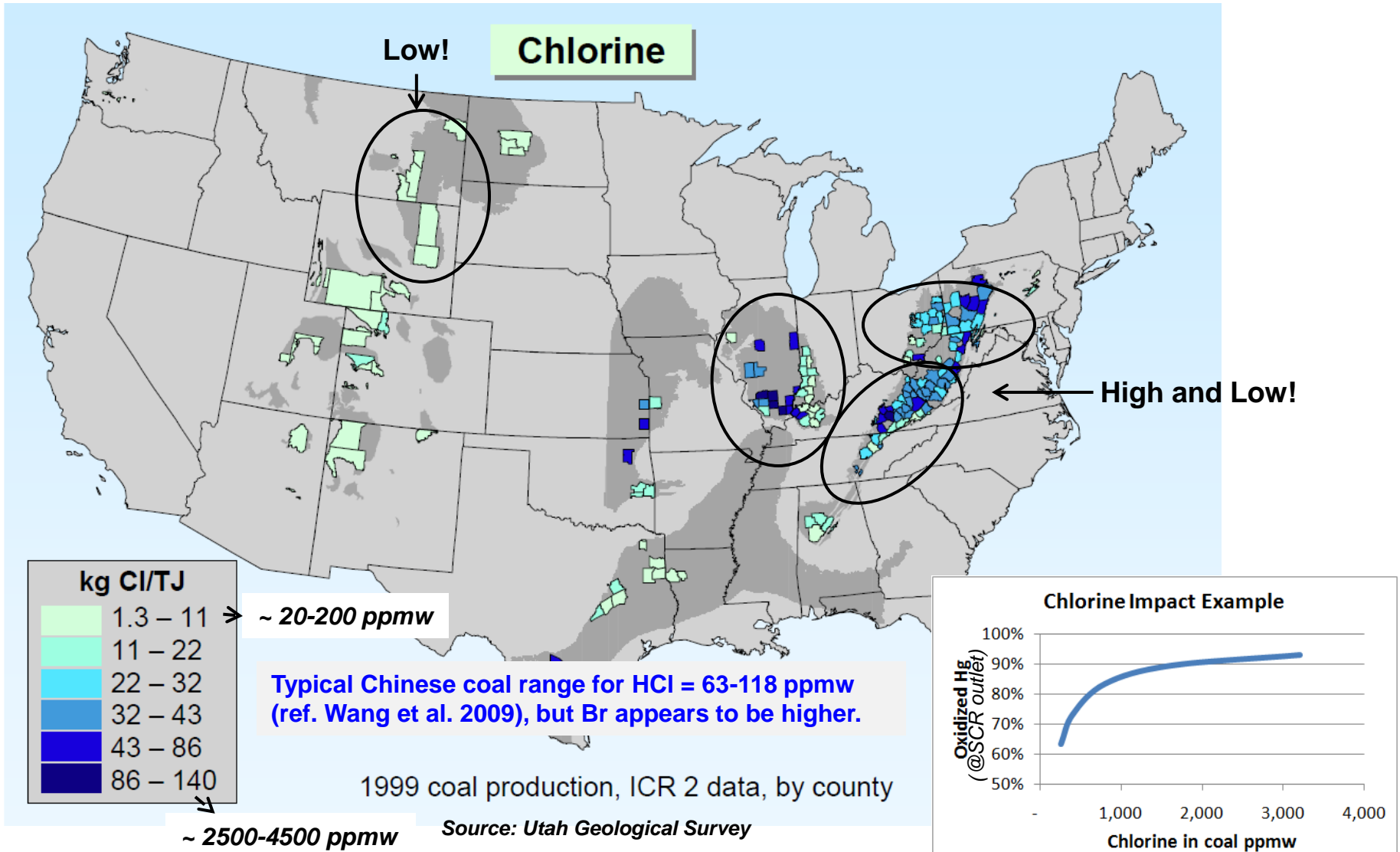
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Key factors: Hg in Coal

(% Removal @ 1.2 lb/TBTU emission)

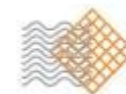


Key factors: Chlorine in Coal



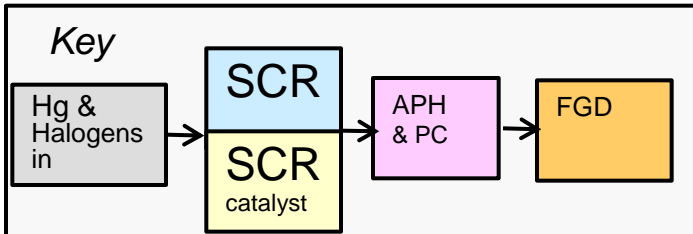
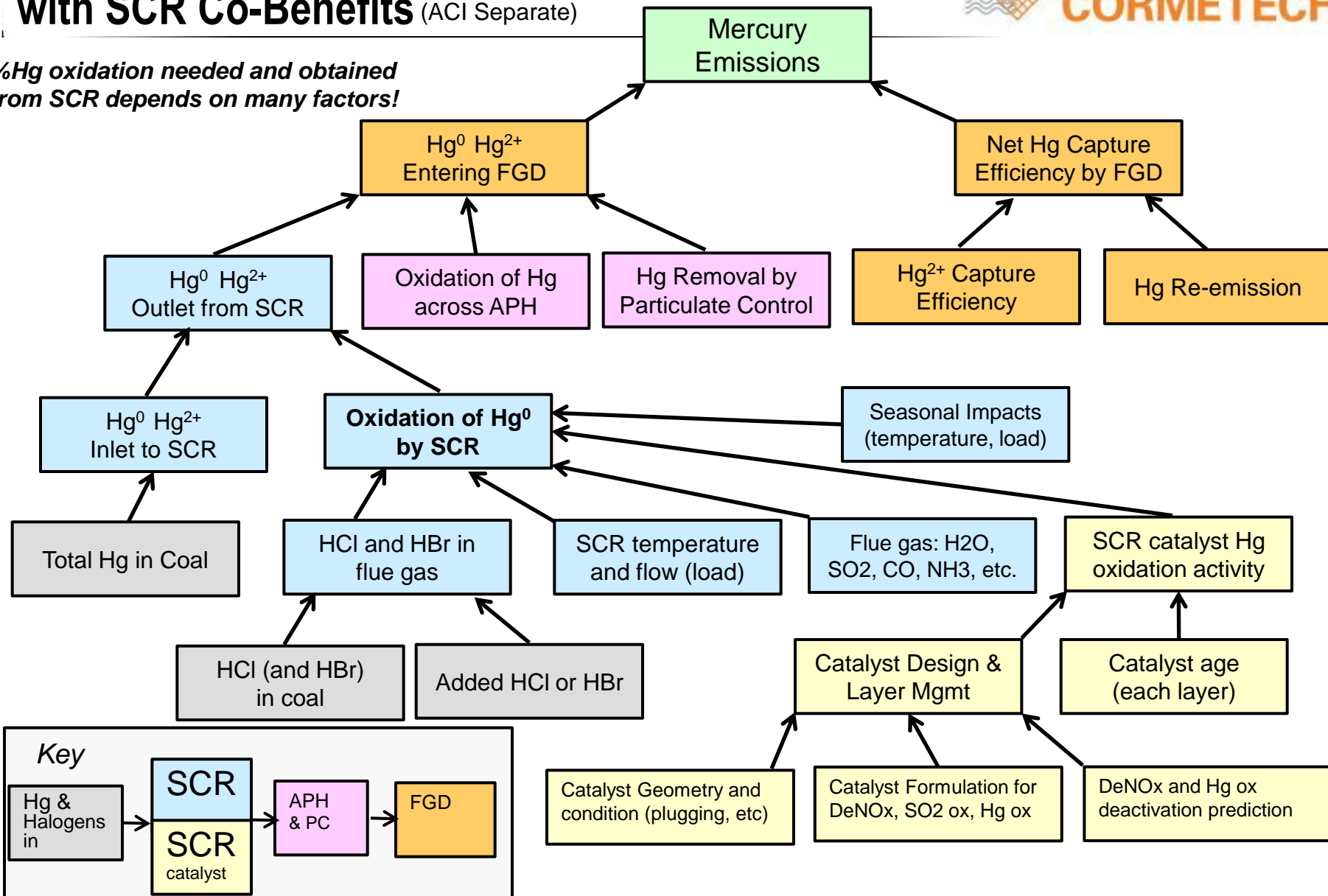
Key Factors Impacting Hg Emissions

with SCR Co-Benefits (ACI Separate)



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%Hg oxidation needed and obtained from SCR depends on many factors!

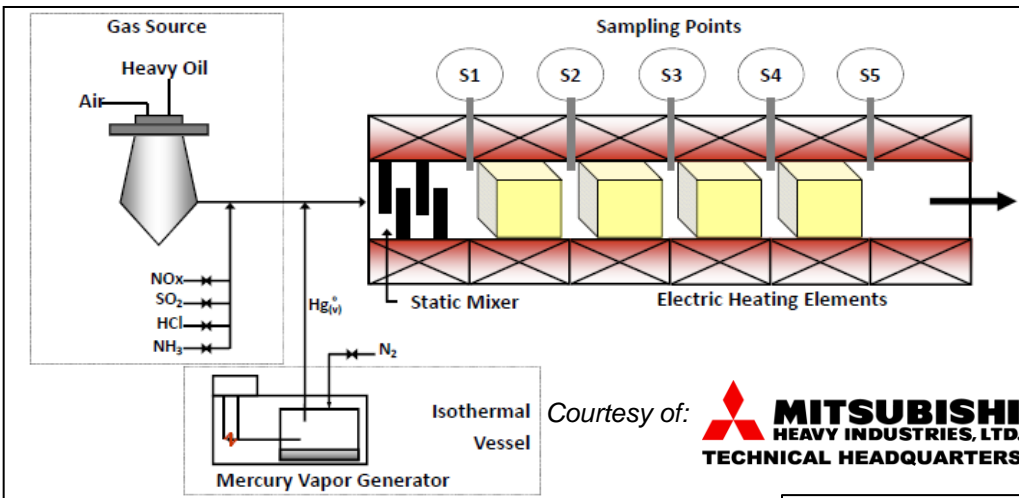


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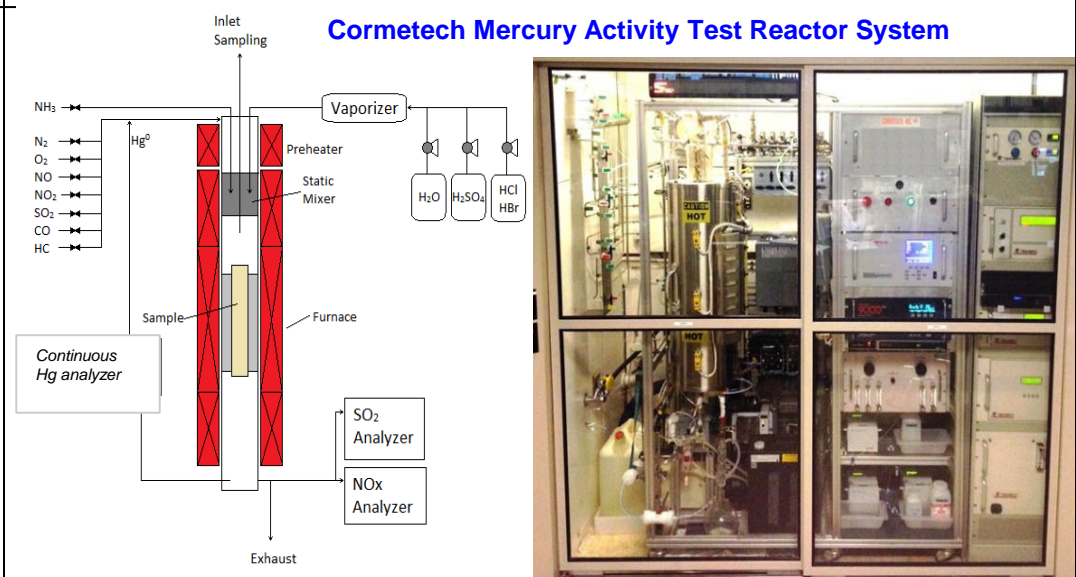
Test Reactor Capabilities



Coming Soon: FALL 2013!
Cormetech pilot reactor with Hg oxidation test capability (reactor can load up to 4 full length/cross-section layers)



- Collected Hg oxidation data for development, designs, deactivation studies, and quality assurance since 2002.
- Allows characterization of catalyst of any type/vintage.



Layer Dependency



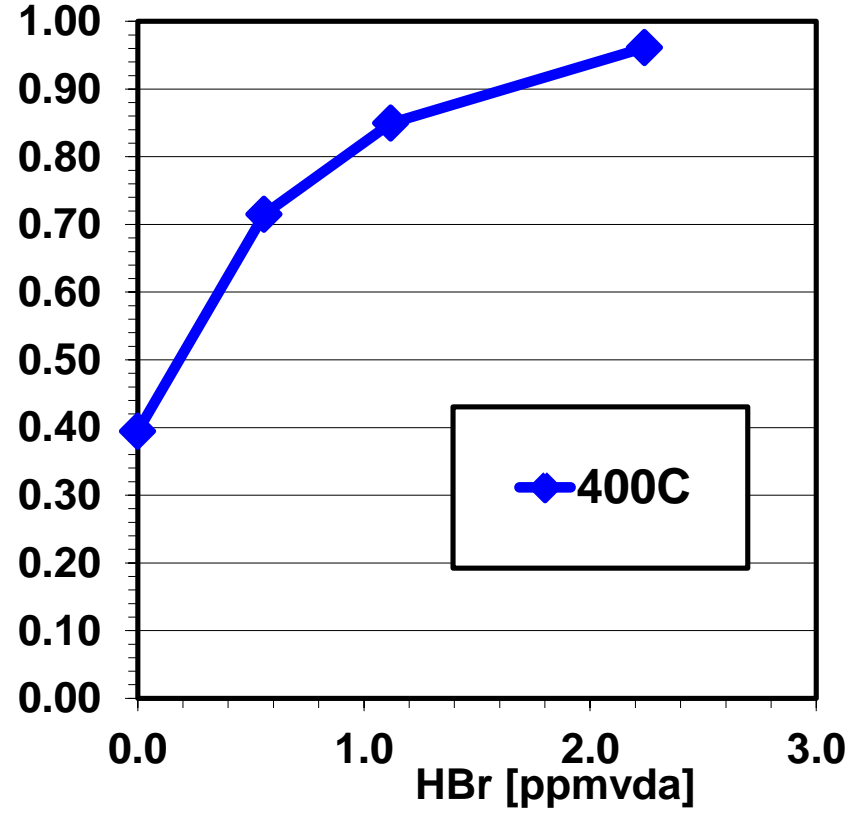
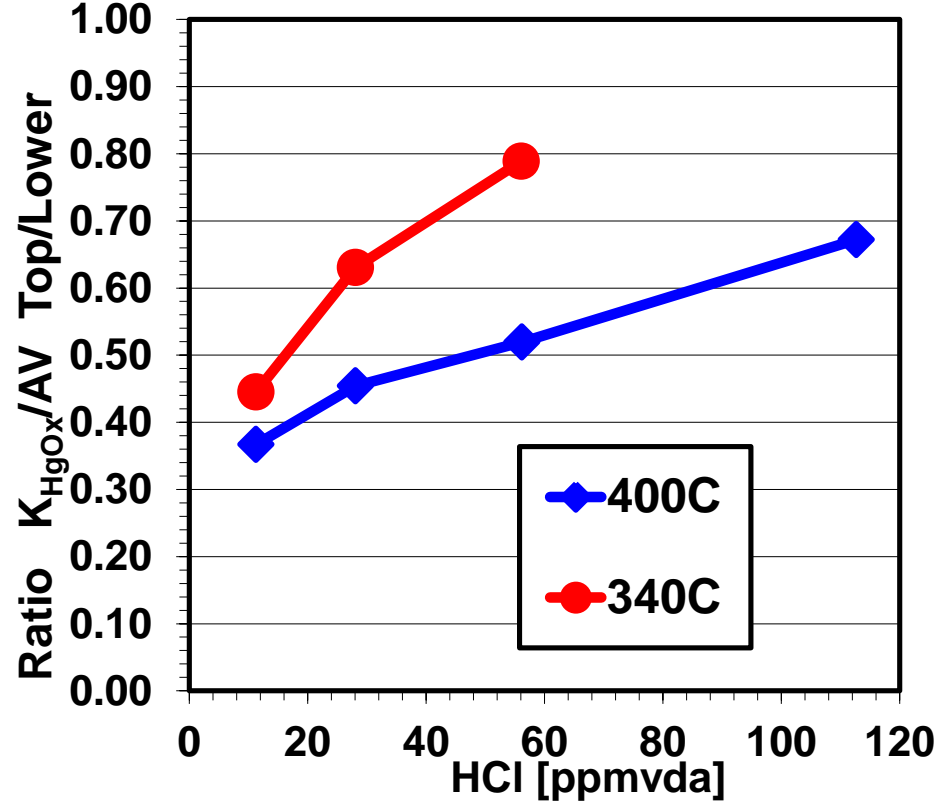
Influenced by Temperature and Halogen Level

$$\frac{K}{AV} = -\ln[1 - \% DeNO_x] \quad \text{For Illustration} \quad \xrightarrow{\text{}} \quad \frac{K_{HgOx}}{AV} = -\ln[1 - \% HgO_x]$$

@ MR=1

$$\frac{K_{HgOx}}{AV} = -\ln[1 - \% HgO_x]$$

f(variable MR)



- Due NH₃ inhibition, Hg oxidation potential depends on layer position.
- The degree of dependency is dependent on temperature and halogen content.

Presentation Outline



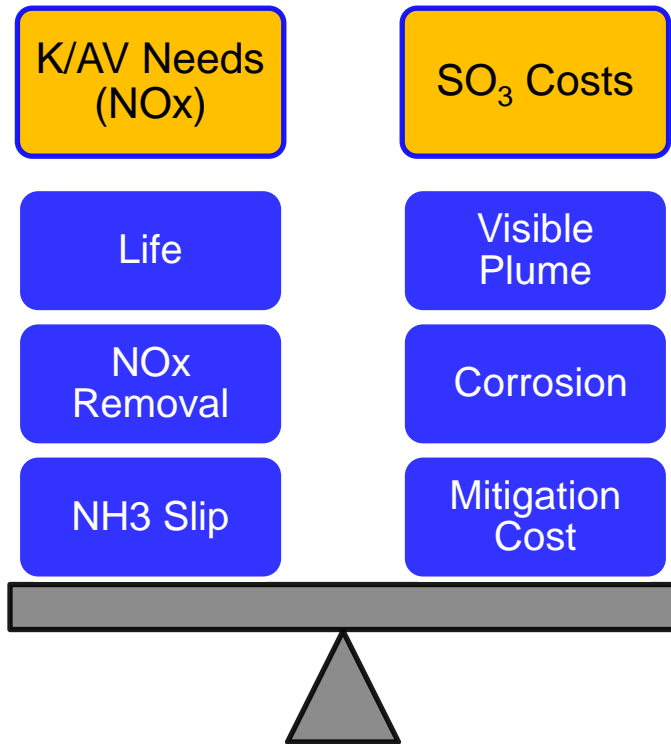
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Catalyst Design Balance



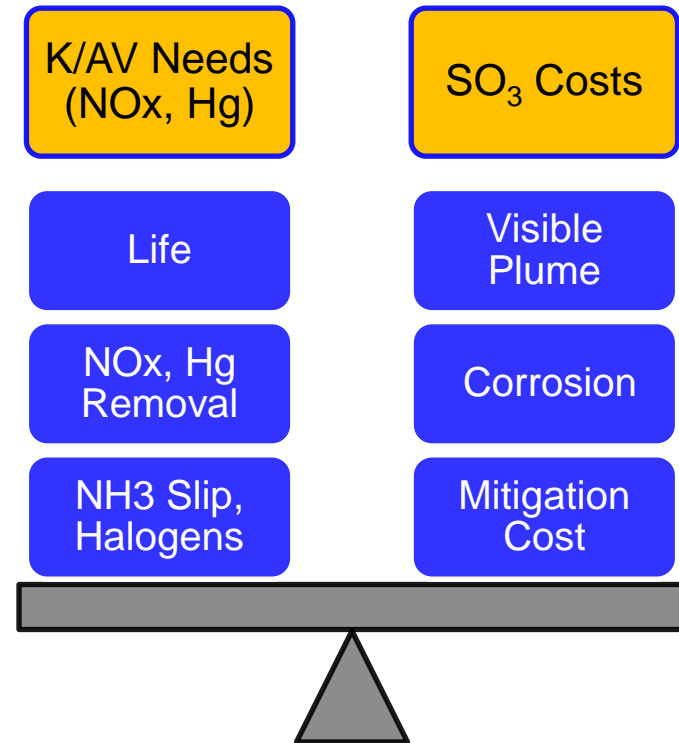
Historical:

Catalyst is formulated to achieve DeNO_x requirements, while meeting SO₂ oxidation constraints.

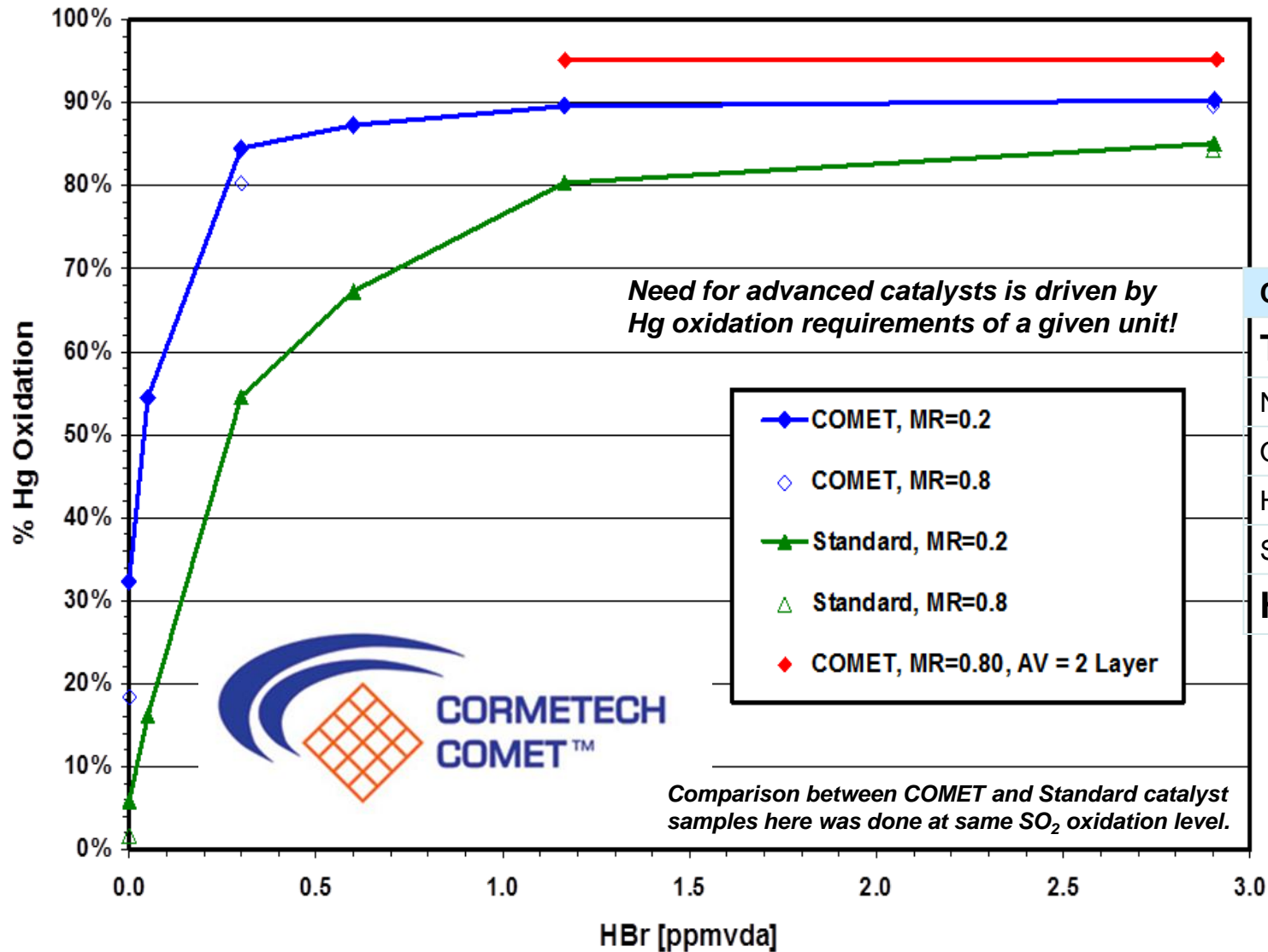


Moving forward:

Catalyst is formulated to achieve DeNO_x and Hg oxidation requirements, while meeting SO₂ oxidation constraints.



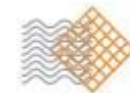
Catalyst Improvements



Constants	
Temp C	403
NOx ppm	107
O2 %	3.5
H2O %	14
SO2 ppm	345
HCl ppm	8



Management Plan w/ DeNOx Potential & Hg Oxidation

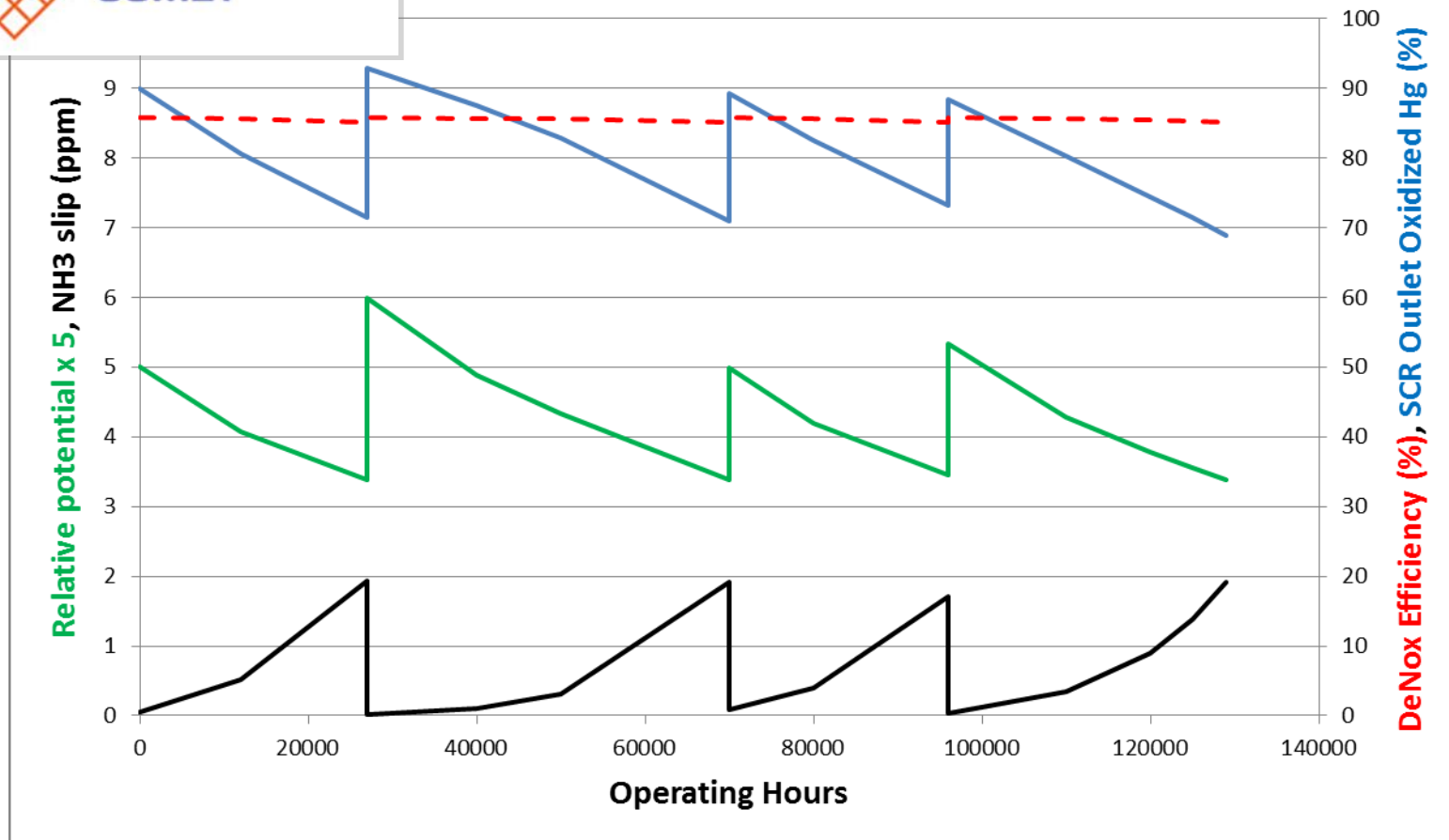


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**Catalyst Management Plan
(DeNox, NH₃ Slip, Oxidized Hg)**

**Performance:
85% DeNOx
Max NH₃ slip = 2 ppm**

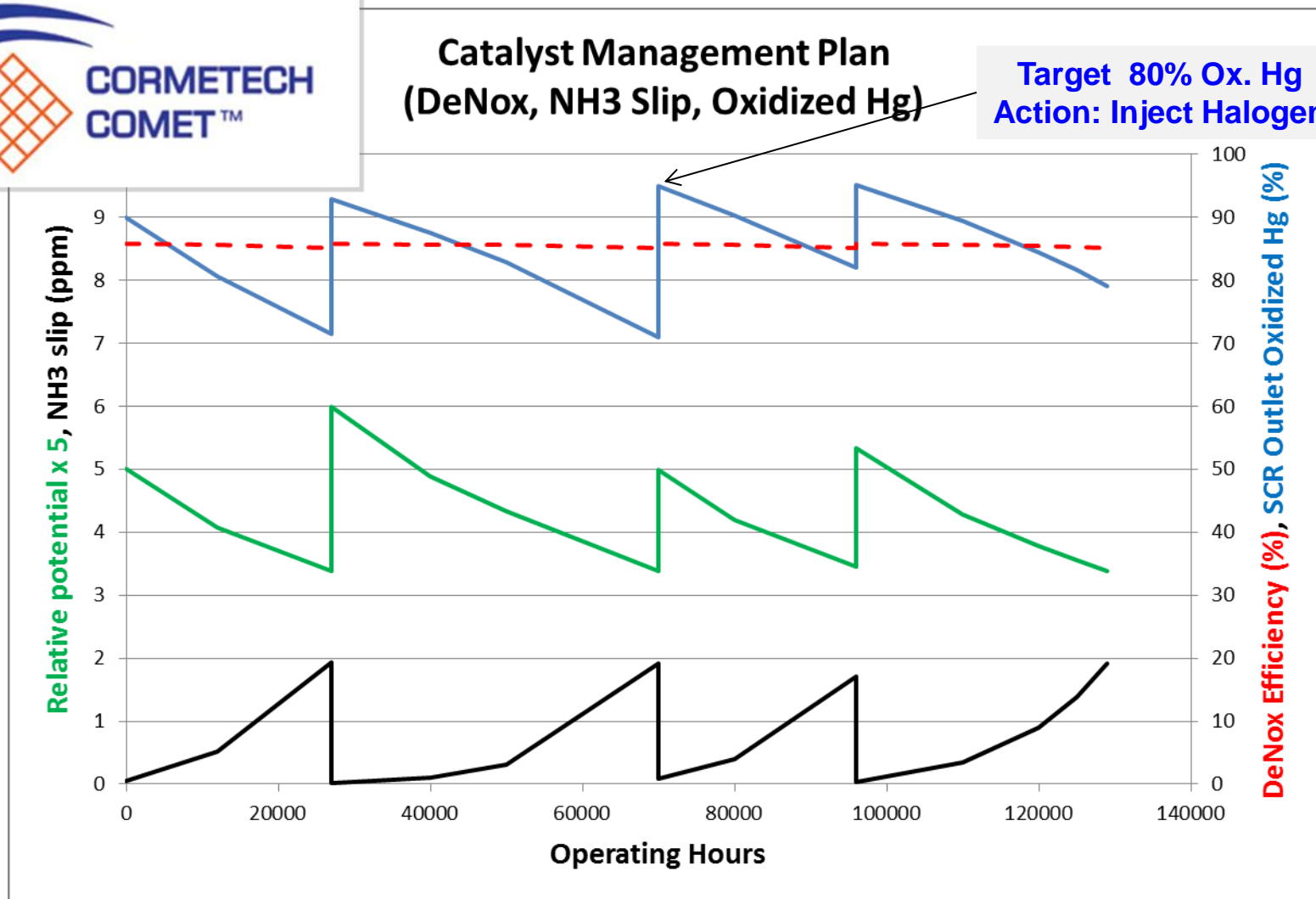


Management Plan w/ DeNOx Potential & Hg Oxidation



**Catalyst Management Plan
(DeNOx, NH3 Slip, Oxidized Hg)**

**Target 80% Ox. Hg
Action: Inject Halogen**

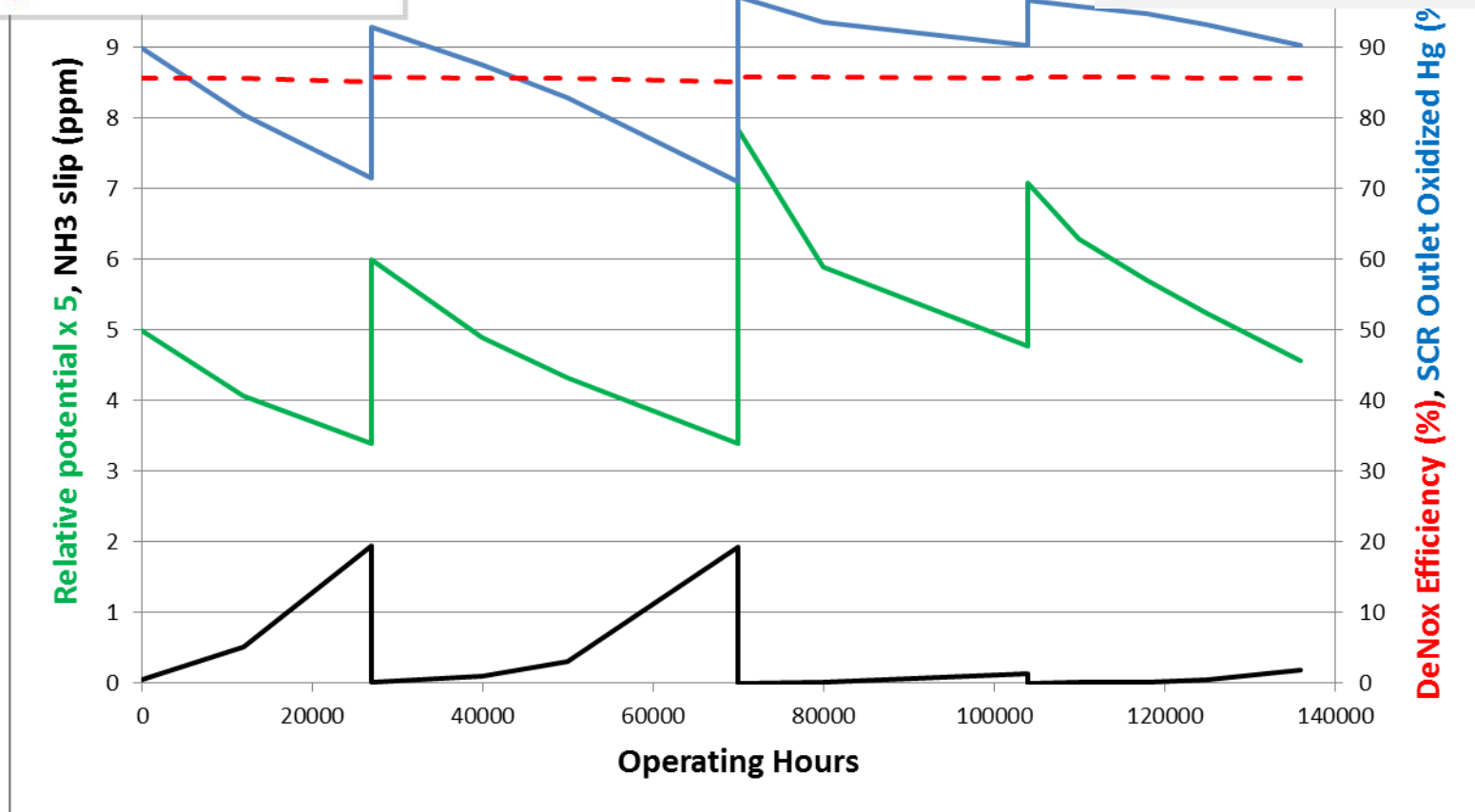


Management Plan w/ DeNOx Potential & Hg Oxidation



**Catalyst Management Plan
(DeNOx, NH3 Slip, Oxidized Hg)**

**Target: 90% Ox. Hg
Action: Initially change
2 layers to Max length
COMET™ and repeat
for layer 3**

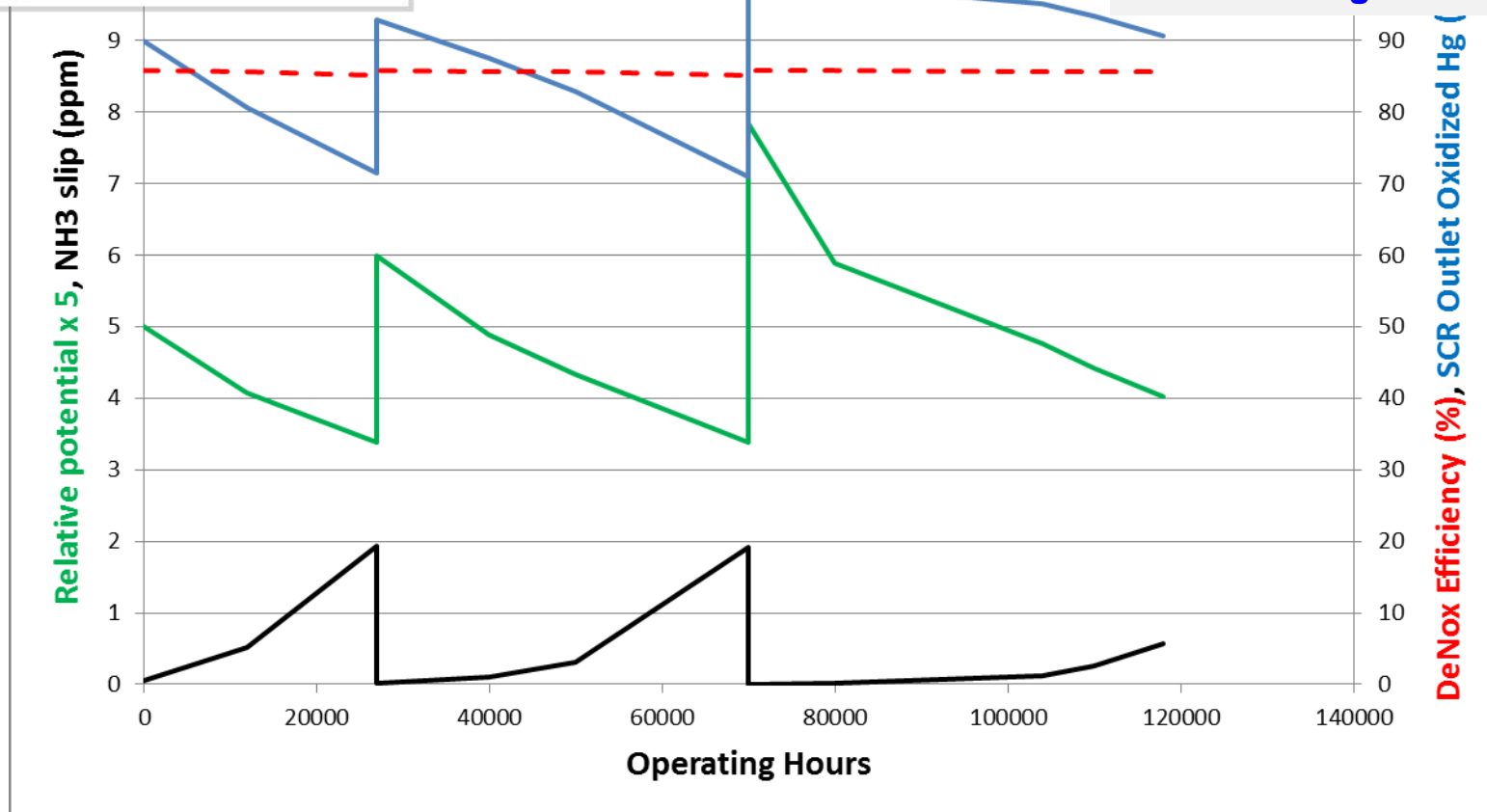


Management Plan w/ DeNOx Potential & Hg Oxidation



Catalyst Management Plan
(DeNOx, NH3 Slip, Oxidized Hg)

Target 90% Ox Hg
Action: Initially change 2
layers to Max length
COMET™ and inject
Halogen



Summary

- Catalyst additions and replacements can be managed to maintain Hg oxidation in a manner analogous to that for DeNO_x, but with a few key differences:
 - **Performance threshold** (dependency on downstream equipment)
 - **Layer dependency**
 - Layer location and NH₃ inlet to each layer must be considered
 - **More factors are needed in setting design conditions**
 - HCl, HBr, CO
 - More significant impacts of Temperature, O₂, and H₂O
- Understanding these dependencies, factors, requires thorough demonstrated testing capability, catalyst technology and application know-how.



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Thank You!

Questions/Discussion

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VGB Workshop “Flue Gas Cleaning 2013”
